Expiration Date: February 24, 2017 Modification Date: January 16, 2019

Lane Regional Air Protection Agency Standard Air Contaminant Discharge Permit

REVIEW REPORT

ADDENDUM NO. 7 Non-NSR/PSD Simple Technical Permit Modification

Hexion Inc. 470 South Second Street Springfield, OR 97477 https://www.hexion.com/ Permit No. 200510

1. <u>General Background Information</u>

Hexion Inc. operates a resin manufacturing facility. Formaldehyde is produced and used primarily on-site as a raw material for various types of resins. Wax emulsions are also produced at this facility. Two (2) tail-gas boilers are used to control Volatile Organic Compounds (VOCs) and Hazardous Air Pollutants (HAPs), while additionally providing steam for the plant. The facility has a number of scrubbers and baghouses used to control other emissions from various portions of the operation. The facility operates 8,760 hours per year (24 hours per day and 365 days per year).

2. Reasons for Permit Action

The facility applied to increase throughput of Durite LV-1259M Loading from 2,250 tons per year to 3,375 tons per year and the Methanol Distillate from 259 tons per year to 777 tons per year. Per LRAPA Title 34-035(1) this is considered a Type 1 modification to the current permit. The emissions from the source will not increase above the PSEL by more than the de minimis emission level defined in LRAPA Title 12. The federally enforceable limits and the TACT determination have been maintained.

3. <u>Projected Emission Increase per Pollutant</u>

Emission Unit	VOC (tpy)	HCHO (tpy)	MeOH (tpy)	Phenol (tpy)	Ethylene Glycol (tpy)	MIBK (tpy)
Durite LV-1259M Loading	0.26	3.58E-03	0.13	2.75E-04	6.08E-06	3.83E-04
Methanol Distillate	0.043	9.61E-04	0.042			
Pre-Project Emissions	0.30	4.54E-03	0.18	2.75E-04	6.08E-06	3.83E-04
Durite LV-1259M Loading	0.38	5.37E-03	0.20	4.12E-04	9.11E-06	5.74E-04
Methanol Distillate	0.13	2.88E-03	0.13			
Post-Project Emissions	0.51	8.25E-03	0.33	4.12E-04	9.11E-06	5.74E-04
Total Emissions Increase	0.21	3.71E-03	0.15	1.37E-04	3.04E-06	1.91E-04

Expiration Date: February 24, 2017 Modification Date: January 16, 2019

4. Projected PSEL

The PSEL are in accordance with Section 42-0040 and 42-0041. The maximum actual emissions are based on the increased throughputs per process using AP-42 Section 5.2 and Section 7.1 emission factors detailed in the facility's Attachment to the Review Report.

Pollutant	Post-Project Facility Emissions (tons/yr)	PSEL
PM	5.88	24
PM ₁₀	5.88	14
PM _{2.5}	5.88	9
СО	14.14	99
NO _X	10.22	39
SO ₂	0.06	39
VOC	47.95	68
Individual HAP	8.72	9
Combined HAPs	20.22	24

5. Typically Achievable Control Technology (TACT)

This permitting action does not change the TACT determination for the facility.

6. New Source Performance Standards (NSPSs)

This permitting action does not change current NSPSs for the facility.

7. National Emissions Standards for Hazardous Air Pollutants

This permitting action does not change current NESHAPs for the facility.

8. Public Notice

In accordance with LRAPA 37-0066(4)(b)(A), as a Non-NSR Simple Technical Permit Modification, Title 31 Category I public notice is required. Category I public notice procedures specify that no prior public notice or opportunity for participation is required.

KE/CMW 01/16/2019

Expiration Date: February 24, 2017 Modification Date: January 16, 2019

Pre- and Post-Construction Emissions Calculations

			Pre-Construction				
Emission Unit		erating ameter	Pollutant	EF	Units	Reference	Emissions (ton/yr)
			VOC	1.14E-04	lb/lb	AP-42 5.2	0.26
			НСОН	1.59E-06	lb/lb	AP-42 5.2	3.58E-03
Durita IV 1250M Loading	2.250	tonohur	MeOH	5.93E-05	lb/lb	AP-42 5.2	0.13
Durite LV 1259M Loading	2,250	tons/yr	Phenol	1.22E-07	lb/lb	AP-42 5.2	2.75E-04
			Ethylene Glycol	2.70E-09	lb/lb	AP-42 5.2	6.08E-06
			Methyl Isobutyl Ketone	1.70E-07	lb/lb	AP-42 5.2	3.83E-04
			VOC	3.33E-01	lb/ton	AP-42 7.1	0.043
Methanol Distillate	259	tons/yr	HCOH	7.42E-03	lb/ton	AP-42 7.1	9.61E-04
			MeOH	3.26E-01	lb/ton	AP-42 7.1	0.042

			Post-Construction				
Emission Unit		erating ameter	Pollutant	EF	Units	Reference	Emissions (ton/yr)
			VOC	1.14E-04	lb/lb	AP-42 5.2	0.38
			НСОН	1.59E-06	lb/lb	AP-42 5.2	5.37E-03
Durite LV 1259M Loading	3,375	tonolur	MeOH	5.93E-05	lb/lb	AP-42 5.2	0.20
Durite EV 1259W Loading	3,375	tons/yr	Phenol	1.22E-07	lb/lb	AP-42 5.2	4.12E-04
			Ethylene Glycol	2.70E-09	lb/lb	AP-42 5.2	9.11E-06
			Methyl Isobutyl Ketone	1.70E-07	lb/lb	AP-42 5.2	5.74E-04
			VOC	3.33E-01	lb/ton	AP-42 7.1	0.130
Methanol Distillate	777	tons/yr	НСОН	7.42E-03	lb/ton	AP-42 7.1	2.88E-03
			MeOH	3.26E-01	lb/ton	AP-42 7.1	0.127

Lane Regional Air Protection Agency Standard Air Contaminant Discharge Permit

REVIEW REPORT

ADDENDUM NO. 6 Non-NSR/PSD Simple Technical Permit Modification

Hexion Inc. 470 South Second Street Springfield, OR 97477 https://www.hexion.com/ **Permit No. 200510**

1. General Background Information

Hexion, Inc. operates a resin manufacturing facility. Formaldehyde is produced and used primarily on-site as a raw material for various types of resins. Wax emulsions are also produced at this facility. Two (2) tail-gas boilers are used to control Volatile Organic Compounds (VOCs) and Hazardous Air Pollutants (HAPs), while additionally providing steam for the plant. The facility also has a number of scrubbers and baghouses used to control other emissions from various portions of the operation. The facility operates 8,760 hours per year (24 hours per day and 365 days per year).

2. Reasons for Permit Action

The facility applied to increase the Urea-Formaldehyde (UF) and Phenol-Formaldehyde (PF) resin production rate to 200,000 tons per year from 140,000 tons per year. This proposed increase to the UF and PF resin production will entail increasing the throughputs of the resin storage, formaldehyde storage, methanol storage, phenol/LPE storage, and urea weigh bins to accommodate the increase of production. In this addendum Hexion is also requesting the removal of the methanol loading because this activity will no longer be done at the facility.

Per LRAPA Title 34-035-2 this is considered a Type 2 modification to the current permit. This emissions have increased, but have not over the current PSELs or over the significant emission rates (SERs). The federally enforceable limits and the TACT determination have been maintained.

3. Description of Throughputs Changes per Processes

Process	Current Throughput (tons/yr)	Increased Throughput (tons/yr)
UF and/or PF/PRF Resin Produced in Reactors	140,000	200,000
Formaldehyde Storage	82,075	100,000
Methanol Storage	45,000	66,000
Phenol/LPE Storage	27,000	40,000
Urea Weigh Bins #1 and #2	25,000 each	50,000 each
Methanol Loading	250	0

Expiration Date: February 24, 2017 Modification Date: July 24, 2017

4. Plant Site Emission Limits

Projected Emission Increase per Pollutant:

Pollutant	PM ₁₀ /PM _{2.5} (tpy)	VOC (tpy)	Methanol* (tpy)	Total HAPs (tpy)
Pre-Project Emissions Totals (140,000 tons)	0.50	23.29	4.27	7.24
PF/UF Resin Production		11.84	1.49	2.55
 PF/UF Resin Storage 		0.45	0.17	0.27
 PF/UF Resin Loading 		7.83	0.89	1.24
 Formaldehyde Storage 		1.69	0.24	1.69
 Methanol Storage 		0.26	0.26	0.26
 Phenol/LPE Storage 		1.18	1.18	1.18
 Urea Bins #1 & #2 	0.50			
 Methanol Loading 		0.04	0.04	0.04
Post-Project Emissions Totals (200,000 tons)	1.00	29.74	5.02	8.60
 PF/UF Resin Production 		11.84	1.85	3.29
PF/UF Resin Storage		0.48	0.19	0.31
PF/UF Resin Loading		11.15	1.28	1.73
Formaldehyde Storage		1.81	0.26	1.81
Methanol Storage		0.26	0.26	0.26
Phenol/LPE Storage		1.18	1.18	1.18
• Urea Bins #1 & #2	1.00			
Emission Increase	0.50	6.45	0.75	1.36
SER	15/10	40	10	25

^{*}Methanol is the individual HAP that has highest emission rate.

Projected PSEL

The PSEL are in accordance with Section 42-0040 and 42-0041. The maximum actual emissions are based on the increased throughputs per process using R&D and AP-42 Section 5.2 and Section 7.1 emission factors.

Pollutant	Post-Projected Facility Emissions (tons/yr)	PSEL
PM	5.88	24
PM ₁₀	5.88	14

Expiration Date: February 24, 2017 Modification Date: July 24, 2017

Pollutant	Post-Projected Facility Emissions (tons/yr)	PSEL
PM _{2.5}	5.88	9
CO	14.14	99
NOx	10.22	39
SO ₂	0.06	39
VOC	47.58	68
Individual HAP	8.48	9
Combined HAPs	19.98	24

5. Typically Achievable Control Technology (TACT)

This permitting action does not change the TACT determination for the facility.

6. New Source Performance Standards (NSPSs)

This permitting action does not change current NSPSs for the facility.

7. National Emissions Standards for Hazardous Air Pollutants

This permitting action does not change current NESHAPs for the facility.

8. Public Notice

In accordance with LRAPA 37-0066-4-B.1, as a Non-NSR Simple Technical Permit Modification, Title 31 Category I public notice is required. Category I public notice procedures specify that no prior public notice or opportunity for participation is required.

BD/cmw 7/18/2017

Attachments

Post-Project Facility Emissions (tpy) 5.88 5.88 5.88 10.22 14.14 0.06 47.58 8.48 19.98 Current PSEL 24 14 9 39 99 39 68 9 24		Post	Post-Project Facility Emissions compared to PSELs	cility Emis	sions comp	ared to PS	ELs			
5.88 5.88 10.22 14.14 0.06 47.58 8.48 14 9 39 99 39 68 9		PM	PM ₁₀	PM _{2.5}	×ON	СО	SO ₂	VOC	Individual	Combined
14 9 39 99 39 68 9	Post-Project Facility Emissions (tpy	5.88	5.88		10.22	14.14	0.06	47.58	8.48	19.98
	Current PSEL	24	14	9	39	99	39	68	9	24
1. Methanol is the individual HAP that has the highest emission rate	1. Methanol is the individual HAP th	nat has the	highest en	nission rate	U					

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otals	eniyiele Giyeoi Storage	hethylene Glycol Storage			GN8/11 Tote Transloading	GN8/11 Loading (MeOH Contribution)	GN8/11 Storage	Washwater Pit	UF Seal Water Storage	PF Washwater/Seal Water Storage	Distillate Storage	Slack Wax Storage	Emusified Wax Storage	Emulsined Wax Loading	Emileified Wax Looding	Emulsified Wax Process	Stearic Acid Storage	Catalyst Loading	RTU Mixer	Adhesive Dump Hopper	Blender 2 - Catalyst Plant	Blender 1 - Fentak	Blender 1 - Catalyst Plant	Road Emissions	Weathernariding	Melamina Handina	Dry Catalyst	Urea Weigh Bin #2 Throughput	Urea Weigh Bin #1 Throughput	Resin Drying Pad Throughput	Miura Boiler No. 2 Natural Gas	Miura Boiler No. 1 Natural Gas	Erie Boiler Tail Gas Usage	Johnston Boiler Natural Gas Usage	Johnston Boiler Tail Gas Usage	Triethanolamin Storage	Monethanolamine Storage	Phenol/LPE Storage	Methanol Stoage	MF Resin Loading	MF Resin Stoage	MF Resin Produced in Reactors	Durite SC-748A Loading	Durite LV-1259M Loading	PF/UF Resin Loading	PF/PRF/UF Resin Storage	PF/UF Resin Produced in Reactors	Triazine Loading	Triazine Storage	Formal debude I pading	Formaldehyde Storage	Finitive Emissions - Desir	Finitive Emissions - Plant 2	Finitive Emissions Bloot 2	Formaldehyde Plant 2 Exhaust Bypass	Formaldahada Blast a Fatta B	Process	
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Expiration Date: February 24, 2017 Modified Date: May 20, 2016

> Lane Regional Air Protection Agency Standard Air Contaminant Discharge Permit

REVIEW REPORT

ADDENDUM NO. 5 Non-NSR/PSD Simple Technical Permit Modification

Hexion Inc. 470 South Second Street Springfield, OR 97477 https://www.hexion.com/

Permit No. 200510

1. General Background Information

Hexion, Inc. operates a resin manufacturing facility. Formaldehyde is produced and used primarily on-site as a raw material for various types of resins. Wax emulsions are also produced at this facility. Two (2) tail-gas boilers are used to control Volatile Organic Compounds (VOCs) and Hazardous Air Pollutants (HAPs), while additionally providing steam for the plant. The facility also has a number of scrubbers and baghouses used to control other emissions from various portions of the operation. The facility operates 8,760 hours per year (24 hours per day and 365 days per year).

2. Reasons for Permit Action

The facility applied to replace the 1,500 horsepower Nebraska tail gas boiler (Boiler-1) with a 1,000 horsepower Johnston tail gas boiler (Boiler-6). Per LRAPA Title 34-035-2 this is considered a Type 2 modification to the current permit. This emissions have increased, but have not over the current PSELs or over the significant emission rates (SERs). The federally enforceable limits and the TACT determination have been maintained.

3. Description of Johnston Tail Gas Boiler

Boiler – 6: Tail Gas boiler – Manufactured by Johnston; rated at 17.6 MMBtu/hr (1,000 horsepower) with a maximum fuel usage of 220,200 scf/hr utilizing tail gases as primary fuel and natural gas as a secondary fuel.

4. Plant Site Emission Limits

The PSEL are in accordance with Section 42-0040 and 42-0041. Maximum actual emissions are based on the estimated maximum MMBtu rating for the Johnston Boiler (Boiler-6) at 8,760 hours per year for tail gas burning and 54 hours per year for bypass per Hexion's ACDP Addendum #3 issued January 6, 2014, and 6 MMscf per year of natural gas use per application for current action. Hexion has evaluated the worst-case emissions between the following available data sources: the existing Nebraska tail gas boiler stack test data from April 2010 and EPA AP-42 emission factors for natural gas boilers. The evaluation of EPA AP-42 included applying the ratio of higher heating value of the tail gas (80 Btu/scf) and average natural gas (1020 Btu/scf) to EPA AP-42 Section 1.4 for natural gas combustion emission factors. Based on Hexion's request, nitrogen oxides (NOx), sulfur dioxide (SO₂), and particulate matter (PM, PM₁₀, PM_{2.5}) emission factors are based on EPA AP-42, and carbon monoxide (CO), volatile organic compounds (VOC), methanol, and formaldehyde emissions will be based on the Nebraska tail gas boiler 2010 stack test data. There is no increase to the current PSEL for this action.

Hexion Inc.

Permit No. 200510

Expiration Date: February 24, 2017 Modified Date: May 20, 2016

Pollutant	New Johnston Boiler Emissions (tons/yr)	Nebraska Boiler Emissions (tons/yr)	Project Increase Emissions*
PM/PM ₁₀ /PM _{2.5}	0.57	- 0.02	0.55
CO	6.35	- 6.62	-0.27
NO _X	7.56	- 0.50	7.05
SO ₂	0.0453	- 0.0176	0.04
VOC	5.48	- 5.48	0.00
Methanol	1.10	- 1.09	0.01
Formaldehyde	0.11	- 0.11	0.00
Total HAP	1.21	- 1.20	0.01

^{*}Project Increase Emissions have not increased the PSEL of the facility.

5. <u>Typically Achievable Control Technology (TACT)</u>

LRAPA Title 32-008 required an existing emission unit at a facility to meet TACT if the emissions unit has emission of criteria pollutants greater than ten (10) tons per year of any gaseous pollutant or five (5) tons per year of particulate, the emissions unit is not subject to the emissions standards under LRAPA Title 32, Title 33, Title 39, or Title 46 for the pollutants emitted, and the facility is required to have a permit. The formaldehyde production lines emit more than ten (10) tons per year of gaseous pollutants and are therefore, required to meet TACT. LRAPA has determined that the tail gas boiler meet TACT for this facility. The emissions from the tail gas boiler emit more than ten (10) tons per year of gaseous pollutants; but because the boiler is subject to the opacity and grain loading limits in Title 32, TACT does not to the boiler.

6. New Source Performance Standards (NSPSs)

The Johnston Boiler (EU: Boiler-6) is subject to Small Industrial – Commercial – Institutional Steam Generating Units. [40 CFR 60 Subpart Dc]

7. National Emissions Standards for Hazardous Air Pollutants

The Johnston Tail Gas boiler is not subject to any NESHAPs.

8. Public Notice

In accordance with LRAPA 37-0066-4-B.1, as a Non-NSR Simple Technical Permit Modification, Title 31 Category I public notice is required. Category I public notice procedures specify that no prior public notice or opportunity for participation is required.

BD/cmw 5/19/2016 Hexion Inc.

Permit No. 200510

Expiration Date: February 24, 2017 Modified Date: May 20, 2016

Attachment

	Nebraska Boi	ler Waste Ta	ail Gas En	nissions		
Nebras	ka Boiler Hours of	Operation		8	760	hrs/yr
Emissio	n (TPY)					
NOx	0.21					
CO	6.37					
VOC	5.46					
Formaldehyde	0.11					
Methanol	1.085					
		Calculation	ns			
Tail Gas Co	mbustion	NOx	СО	VOC	НСНО	MeOH
Emission Fac	ctors (lb/hr)	0.05	1.45	1.25	0.02507	0.25
Concentrat	ions used	Outlet	Inlet	Inlet	Inlet	Inlet

Notes: Stack Test Data was used for the Emission Factors for the Nebraska Boiler. NOx used the outlet (lb/hr) data of the outlet concentration and CO, VOC, HCHO, and MeOH used the inlet concentrations with a 94% capture efficiency for CO and 99.5% capture efficiency the VOC, Formaldehyde and Methohal

Hexion Inc.

Permit No. 200510
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Source:	Nebraska Boiler			
		natural gas combustion a		3
2. The AP-	42 emission factors fo	r SOx was assumed for SO	2	
	D	Permit Basis		
	Description	Quantity	Units	
	s Heating Value	1,000	Btu/scf	
	Natural Gas Usage	6	MMscf/yr	
Conversio	n Factor	2,000	lb/ton	
		EMISSION FACTORS		
	AP-4	12 Table 1.4-1 and 1.4-2		
Emi	ssion Factors for Crite	ria Pollutants from Natura	al Gas Combustion	
	Component	Emission Factor	or (lb/MMScf)	
VOx		10	00	
0			4	
SOx			.6	
PM10			.6	
/OC			.5	
Based on a	heating value of	1020	Btu/scf	
	Annual	Hours of Operation: 8760	1	
	Calculation	s for Nebraska Boiler Ta	ail Gas Combustion Em	issions
Calcu	late the Criteria Pollu	tants Emissions and Speci	ated VOC Emissions	
Natural	Gas Heating Value	Natural Gas Usage	Conversion Factor	
	Btu/scf	MMscf/yr	lb/ton	
	1,000	6	2,000	
		AP-42 EF	Annual Emissions ¹	Annual Emissions ²
	Component	lb/MMscf	(lb/yr)	(tpy)
Юx		100	588	0.29
0		84	494	0.25
		0.60	4	0.0018
02				
O2 PM10 /OC		7.60	45	0.02

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Speciated VOC Emission Calculations

Component	AP-42 EF	Annual Emissions ¹	Annual Emissions ²
	lb/MMscf	(lb/yr)	(tpy)
Benzene	2.10E-03	1.24E-02	6.18E-06
Dichlorobenzene	1.20E-03	7.06E-03	3.53E-06
Formaldehyde	7.50E-02	4.41E-01	2.21E-04
Hexane	1.80E+00	1.06E+01	5.29E-03
Naphthalene	6.10E-04	3.59E-03	1.79E-06
Toluene	3.40E-03	2.00E-02	1.00E-05
Polycyclic Organic Matter	8.82E-05	5.19E-04	2.59E-07
Non-HAP/TAP VOC	9.40E+00	5.53E+01	2.76E-02
Total Speciated VOC		6.64E+01	3.32E-02

Formulas Nebraska Boiler:

- 1. Emissions (lb/yr) = AP-42 Emission Factor (lb/MMscf)*[(1,000 btu/scf NG)/scf NG Average)]* Natural Gas Usage (MMscf/yr)
- 2. Annual emissions (tpy) = Average emissions (lb/yr) /Conversion Factor (lb/ton)

For the Johnston Boiler Emissions

- 1. Natural Gas is only used for pilot gas.
- 2. Emissions (lb/yr) = AP-42 Emission Factor (lb/MMscf)*[(1,000 btu/scf NG)/scf NG Average)]* Natural Gas Usage (MMscf/yr)
- 3. Annual emissions (tpy) = Average emissions (lb/yr) /Conversion Factor (lb/ton)

EMISSIO	N FACTORS
AP-42	Table 1.4-3
Emission factors for Spe	ciated Organic Compounds
from Natural	Gas Combustion
	Emission Factor
Component	(lb/MMScf)
Benzene	2.10E-03
Dichlorobenzene	1.20E-03
Formaldehyde	7.50E-02
Hexane	1.80E+00
Naphthalene	6.10E-04
Toluene	3.40E-03
Polycyclic Organic	
Matter	8.82E-05

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		בליווינים בכותי	יייייייייייייייייייייייייייייייייייייי	missions	
Source: John	Johnston Boiler				
Assumptions:					
1. For the purposes of preparing a Type 2 NOI application, Hexion has evaluated the worst case	paring a Type 2 NOI a	pplication, Hexion	as evaluated the worst c	ase emissions between the	emissions between the only available data sources
2. The AP-42 emission factors for SOx was assumed for SO2	tors for SOx was assu	med for SO2	ימווט או אב כווווטטוטוו ומני	ors for flatful al 84s politers	
	Permit Basis				
Description	Quantity	Units			
Tail Gas Heating Value	80	Btu/scf			
Conversion Factor	2,000	lb/ton			
EN	EMISSION FACTORS			EMISSIC	EMISSION FACTORS
AP-42	AP-42 Table 1.4-1 and 1.4-2			AP-42	AP-42 Table 1.4-3
Emission Factors for	Emission Factors for Criteria Pollutants from Natural Gas	om Natural Gas		Emission factors for Specia	Emission factors for Speciated Organic Compounds from
	Combustion			Natural Ga	Natural Gas Combustion
Component	Emission Fact	Emission Factor (lb/MMScf)		Component	Emission Factor (lb/MMScf)
NOx	1	100		Benzene	2.10E-03
CO		84		Dichlorobenzene	1.20E-03
SOx	0	0.6		Formaldehyde	7.50E-02
PM10	7	7.6		Hexane	1.80E+00
VOC	5	5.5		Naphthalene	6.10E-04
Based on a heating value of	of 1020 I	1020 Btu/scf		Toluene	3.40E-03
				Polycyclic Organic Matter	8.82E-05
Annual H	Annual Hours of Operation: 8760	760		Non-HAP/TAP VOC	9.40E+00

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	Calcu	lations for Johnstor	Calculations for Johnston Boiler Tail Gas Combust
Emission Calcul	Emission Calculations using AP-42 Section 1.4	Section 1.4	
Tail Gas Heating Value	Boiler Heat Input	Conversion Factor	
Btu/scf	MMBtu/hr	lb/ton	
80	17.6	2,000	
Component	Tail Gas EF	Annual Emissions ¹	Annual Emissions ²
00110110	lb/MMBtu	(lb/yr)	(tpy)
NOx	0.098	15,115	7.56
CO	0.082	12,697	6.35
SO2	0.001	91	0.045
PM10	0.007	1,149	0.57
VOC	0.005	831	0.42
Emission Calculations using the Nebraska Boiler 2010 Stack Test Data	g the Nebraska Boi	er 2010 Stack Test Dat	a
Component	Tail Gas Combustion Factor	Johnston Boiler Annual Emission	
	lb/hr	tpy	
NOx	0.050	0.22	
CO	1.450	6.35	
Total VOC	1.250	5.48	
Formaldehyde	0.025	0.11	

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	Johnston Boiler		
Component	Annual Emission		
	tpy		
NOx	7.56		
CO	6.35		
SO2	0.05		
PM/PM10/PM2.5	0.57		
Total VOC	5.48		
Formaldehyde	0.11		
Methanol	1.10		
	AP-42 EF	Applications 1	
00110110	lb/MMscf	(lb/yr)	(tpy)
Benzene	2.10E-03	1.24E-02	6.18E-06
Dichlorobenzene	1.20E-03	7.06E-03	3.53E-06
Formaldehyde	7.50E-02	4.41E-01	2.21E-04
Hexane	1.80E+00	1.06E+01	5.29E-03
Naphthalene	6.10E-04	3.59E-03	1.79E-06
Toluene	3.40E-03	2.00E-02	1.00E-05
Polycyclic Organic Matter	8.82E-05	5.19E-04	2.59E-07
Non-HAP/TAP VOC	9.40E+00	5.53E+01	2.76E-02
Total Speciated VOC		6.64E+01	3.32E-02
Formulas:			
1. Emissions (lb/hr) = $AP-42$	Emission Factors	(lb/MMscf)*[(80 Btu/sc	1. Emissions (lb/hr) = AP-42 Emission Factors (lb/MMscf)*[(80 Btu/scf tail gas)/(1020 Btu/scf NG)/(80 Btu/scf tail gas)] * Heat Input (MMBtu/hr) *

Annual Hours of Operation (hr/yr) 1. Eliissioiis (10/111) = Ar-42 Eliissioii ractors (10/10/10/180 Btd/scr tali gas)/(10/00 Btd/scr tali gas)] * Heat Input (MMBtu/hr) *

^{2.} Annual emissions (tpy) = Average emissions (lb/hr) * Annual hours of operation (hr/yr) / Conversion Factor (lb/ton)

^{3.} VOC emission rates assume a 99.5% control efficiency. CO emission rate assumes a 94% control efficiency.

gas combustion: the existing Nebraska boiler stack test data and AP-42 emission factors for natural gas boilers. 4. For purpost of preparing a Type 2 NOI aplication, Hexion has evaluated that worst cast emissions between the only available data sources for tail

		Project Increas	Project Increases for Nebraska Boiler Replacement	r Replacement		
Pollutant	New Johnston Boiler Emissions (tpy)	Nebraska Boiler Emissions (tpy)	Project Increases (typ)	Facility-wide Pre- Project Emissions (tpy)	Facility-wide Post- Project Emissions (tpv)	PSEL
PM	0.57	-0.02	0.55	5	6	24
PM10	0.57	-0.02	0.55	5	6	14
PM2.5	0.57	-0.02	0.55	5	6	9
NOx	7.56	-0.50	7.05	10	17	39
CO	6.35	-6.62	-0.27	19	19	99
VOC	5.48	-5.48	0.00	50	50	68
S02	4.53E-02	-1.76E-03	0.04	0	0	39
Methanol	1.10	-1.09	0.01	9	9	9
Formaldehyde	0.11	-0.11	0.00	6	6	9
Total HAPs	1.21	-1.20	0.01	18	18	24

Lane Regional Air Protection Agency Standard Air Contaminant Discharge Permit

REVIEW REPORT

Momentive Speciality Chemicals, Inc.

Permit No. 200510

1. <u>General Background Information</u>

Momentive Specialty Chemicals, Inc., located at 470 South Second Street in Springfield, is a resin manufacturing facility. Formaldehyde is produced and used primarily on-site as a raw material for various types of resins. Wax emulsions are also produced at this facility. Two (2) tail-gas boilers are used to control Volatile Organic Compounds (VOCs) and Hazardous Air Pollutants (HAPs), while additionally providing steam for the plant. The facility also has a number of scrubbers and baghouses used to control other emissions from various portions of the operation. Total annual resin production at the facility is approximately 586 million pounds. The facility operates 8,760 hours per year (24 hours per day and 365 days per year).

2. Reasons for Permit Action

The facility operates a process listed in Title 37, Table 1, Part B, and is therefore required to obtain a permit. The facility's permit expired on September 15, 2011. The primary reason for this permit action is to renew the expired permit. The facility requested and LRAPA approved an extension to submit the renewal application. The facility submitted the renewal application and the expired permit was administratively continued until the renewal was approved and issued.

3. <u>Enforcement History</u>

The facility was issued Notice of Non-Compliance (NON) No. 3269 on February 22, 2011 and Notice of Civil Penalty (NCP) No. 11-3269 on April 11, 2011 for installing a new source of air contaminant emissions (Miura boilers) without first notifying LRAPA in writing and obtaining approval. A civil penalty of \$1,500 was imposed by the NCP. In response to request from the facility, the penalty was reduced to \$750 on the basis of amended civil penalty matrix inputs. The facility paid the penalty on May 5, 2011 and the file was closed.

The facility was issued NON No. 2920 on March 19, 2007 and NCP No. 07-2929 for failure to operate the methanol tank farm scrubber in accordance to conditions submitted in the permit application; failure to operate the methanol tank farm scrubber in accordance to conditions submitted in Operation and Maintenance (O&M) plan. A civil penalty of \$1,000 was imposed by the NCP. The facility and LRAPA entered into Stipulated Final Order (SFO) No. 07-2920 to resolve the violation in January of 2008. In response to request from the facility, the penalty was reduced to \$800 on the basis of amended civil penalty matrix inputs. The facility paid the penalty on January 25, 2008 and the file was closed.

The facility was issued NON No. 2366 on March 19, 2002, for failure to operate plant process in accordance with permit application (failed to include emission point V-7, failed to report accurate formaldehyde process, and storage tank temperatures); failure to operate, maintain and demonstrate that plant process scrubbers are operated and maintained at all times in a manner which shall minimize air contaminant discharges; failure to report breakdown of equipment or air pollution control equipment which may result in exceeding permitted emission limits (process scrubbers); and failure to notify and receive approval for modification of Formaldehyde Plant #3. The facility removed tank V-7 and completed the requirements in SFO-02-2366 and the file was closed.

The facility was issued NON No. 1516 on March 3, 1998, and NCP No. 98-1516 on June 8, 1998,

for failure to demonstrate compliance with Leak Detection and Repair (LDAR) requirements.

The facility was also issued NON No. 1519 on March 3, 1998, for failure to comply with New Source Performance Standards (NSPS) Subpart III. No civil penalty was issued, compliance was obtained and the file has been closed.

4. Performance Test Results

The inlets and outlets of Boiler 1 (Nebraska) and Boiler 2 (Erie) were tested on April 27-28, 2010 for VOC, CO, NO_x, Methanol and Formaldehyde. The results were used in establishing revised emission factors for Plant Site Emission Limit (PSEL) compliance.

The Formaldehyde Tank Farm Scrubbers were tested in June of 1991. The current application assumes the tanks are uncontrolled, therefore the test results are not used to estimate emissions. In 2001, the facility performed an emission study on the scrubbers of the reactors at the facility. The emission factors determined by this study are used for the emissions from the scrubbers.

A compliance test was performed on the Boiler 1 (Nebraska Boiler) in March of 1993. For VOC (measured as total organic compounds (TOC)), the boiler tested at greater than the 98% destruction efficiency as required by the New Source Performance Standards (NSPS) Subpart III.

The Methanol Scrubber System was tested in September of 1995. The results showed an average methanol removal efficiency of 99.995%. The current application assumes the system operates at 95% efficiency.

The permit contains emission factor verification testing requirements for the Boiler1 (Nebraska), and the Boiler 2 (Erie).

5. Plant Site Emission Limits

Baseline Emissions Rate (BER) and Significant Emission Rate (SER) Comparison

The baseline emission rates were established in a previous permit issuance and were based on equipment and production totals for the year 1978. The equipment in operation during the baseline year were:

- 1 uncontrolled formaldehyde production line (Plant #2, Erie Boiler), and
- 7 resin kettles, which had controls only on the condensers.

Expiration Date: February 24, 2017

		Netting	g Basis	Plant Site	e Emission Lim	nit (PSEL)	
Pollutant	Baseline Emission Rate (tons/yr)	Previous (tons/yr)	Proposed (tons/yr)	Previous PSEL (tons/yr)	Proposed PSEL (tons/yr)	PSEL Increase over netting basis (tons/yr)	SER (tons/yr)
РМ	3.7	3.7	3.7	24	24	20.3	25
PM ₁₀	3.7	3.7	3.7	14	14	10.3	15
PM _{2.5}	NA	NA	3.7	NA	9	5.3	10
со	7.1	7.1	7.1	37	99	91.9	100
NO _X	28.2	28.2	28.2	24	39	10.8	40
SO ₂	13.5	13.5	13.5	23	39	25.5	40
voc	48.8	48.8	48.8	68	68	19.2	40
GHG	NE	NE	NE	NA	74,000	74,000	75,000

- 5.a. The baseline emission rates for PM, PM₁₀, CO, NO_X, SO₂, VOC and Pb were determined in previous permitting actions and there are no changes. A baseline emission rate is not required for PM_{2.5} in accordance with the definition of "baseline emission rate" in LRAPA Title 12 (see 5.d and 5.e below).
- For greenhouse gases (GHG), NE = Not established. A baseline emission rate was not established with this permitting action due to the relatively low actual emission levels and a facility request to not establish the GHG Baseline Emission Rate.
- 5.c. The PSEL for PM, PM₁₀, PM_{2.5}, NO_X, CO, SO₂ and GHG are established at the Generic PSEL level in accordance with Section 42-0040-1.
- The $PM_{2.5}$ netting basis is established with this permitting action as being equivalent to the PM_{10} netting basis. The fraction of PM_{10} in the netting basis that is $PM_{2.5}$ is assumed to be 100%. The PM from boiler combustion in the baseline year is assumed to be 100% $PM_{2.5}$.
- 5.e. GHG and PM_{2.5} are new regulated pollutants and, therefore, a PSEL for GHG and PM_{2.5} are established with this permit action. The PSEL for PM_{2.5} is established using the procedure specified in the definition of "netting basis" in LRAPA Title 12 (see detail sheets).
- 5.f. There are no Unassigned Emissions and no Emission Reduction Credits available to this facility.

The Attachment to this Review Report contains the calculations of the PSELs.

6. Other Emission Limitations

LRAPA's process weight rule specifies limits on the emissions of particulate matter for specific processes as a function of the amount of material processed. [LRAPA 32-045(A)] This rule is intended for large sources of PM such as wood products facilities. Since PM emissions from the facility are from the combustion of fuel and are relatively small, the facility is expected to be in compliance with the process weight rule.

The permit includes general visible emissions limitations for the facility as well as general grain-loading limitations for the facility.

7. <u>Hazardous Air Pollutants (HAPs)</u>

The facility is required to calculate emissions of HAPs on a 12-month rolling basis. Emissions of total HAPs are expected to be approximately 18.5 tons per year. The attachment to this report contains the calculations of the HAPs.

Pollutant	Emissions (tons/yr)
Formaldehyde	6.00
Methanol	9.42
Phenol	0.70
Ethylene Glycol	0.17
Toluene	0.7
Triethylamine	0.72
Total HAPs (including other HAPs not listed above)	17.9

There are no National Emission Standards for HAPs (NESHAPs) that are applicable to the facility. The facility is not subject to the Chemical Manufacturing NESHAP (Subpart VVVVVV or 6V) because the facility asserts that it does not use or produce any of the 15 HAPs listed in the NESHAP that would make the facility subject. The provisions of the area source boiler NESHAP (Subpart JJJJJJ or 6J) do not include any requirements for gas-fired boilers of any size and therefore the standards, tune-up and energy assessments requirements do not apply to the facility's boilers.

The facility requested that LRAPA add a federally enforceable permit condition (Condition 20) requiring the facility to meet Leak Detection and Repair (LDAR) monitoring requirements pursuant to 40 CFR §§63.162- §63.180 for Plant #2 and Plant #3 and the recordkeeping and reporting requirements of 40 CFR 60, Subpart VV (Condition 19.j and 19.k) for Plant #3.

Momentive Specialty Chemicals, Inc. Permit No. 200510 Expiration Date: February 24, 2017

8. <u>Typically Achievable Control Technology</u> (TACT)

LRAPA Title 32-008 requires an existing emission unit at a facility to meet TACT if the emissions unit has emissions of criteria pollutants greater than 10 tons per year of any gaseous pollutant or five (5) tons per year of particulate, the emissions unit is not subject to the emissions standards under LRAPA Title 32, Title 33, Title 39, or Title 46 for the pollutants emitted, and the facility is required to have a permit. The formaldehyde production lines emit more than ten (10) tons per year of gaseous pollutants and are, therefore, required to meet TACT. LRAPA has determined that the tail gas boilers, scrubbers and baghouses meet TACT for this facility. The emissions from the boilers, as steam-generating units, emit more than 10 tons per year of gaseous pollutants; but because the boilers are subject to the opacity and grain loading limits in Title 32, TACT does not apply to the boilers.

9. New Source Review (NSR) and Prevention of Significant Deterioration (PSD)

Because the proposed PSELs for all regulated pollutants are below the Significant Emission Rates (SERs) in LRAPA Title 38, the facility is not subject to LRAPA's New Source Review (NSR) requirements for PM_{10} nor the Prevention of Significant Deterioration (PSD) requirements for SO_X , NO_X , CO, and VOC.

10. <u>New Source Performance Standards (NSPSs)</u>

The Nebraska tail-gas boiler on Plant #3 was installed in 1990 and since it was constructed after October 21, 1983, the air oxidation reactor and any recovery system it vents to are subject to NSPS Subpart III, Standards of Performance for VOC Emissions from the Synthetic Organic Chemical Manufacturing Industry (SOCMI) Air Oxidation Unit Processes. The permit contains requirements from the NSPS Subpart III. The facility has performed the initial compliance test in accordance with 40 CFR 60.8(a). The permit retains the testing requirements in the event the facility performs or is required to perform additional compliance testing.

Because Plant #3 was modified after January 5, 1981, and is considered part of the SOCMI unit, the equipment of Plant #3 as established, is subject to the New Source Performance Standards Subpart VV, Standards of Performance for Equipment Leaks of VOCs in the SOCMI.

Boilers 4 and 5 (Miura Boilers) each have a maximum design rate of less than 10 MM BTU/hr and are, therefore, **not** subject to the NSPS Subpart Dc.

11. Reporting Requirements

The facility is required to submit semi-annual reports by the 45th day of each semi-annual period for every semi-annual period this permit is in effect, a copy of a report which includes the following information for the preceding semi-annual period (all totals are required to be 12-month rolling totals and expressed in tons per year). The semi-annual periods are defined as January through June and July through December. [LRAPA 34-120]

- a. Estimation of:
 - i. Total VOC, CO, NOx, SO2 and PM/PM₁₀/PM_{2.5}
 - ii. Total HAP and
 - iii. Individual HAP emissions

(The facility is required to use the emission factors specified in the facility's application when determining total VOC, HAP and individual HAP emissions).

b. The parameters required by Permit Condition 24.

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- c. The 12-month rolling total emissions estimations are also to include the estimation of emissions from storage tanks.
- d. The format of the semi-annual report and associated calculations may be required to be modified subject to LRAPA approval.
- e. The annual report is required to contain the GHG emissions in accordance with ODEQ Division 215 GHG reporting rule.

Unless otherwise specified, all reports, test results, notifications, etc., required by the above terms and conditions are to be reported to the following office:

Lane Regional Air Protection Agency 1010 Main Street Springfield, Oregon 97477 (541) 736-1056

The facility is also required to report any entries in the upset log as required per Condition G15.

12. Public Notice

The draft permit was on public notice from January 18, 2012 to February 21, 2012. No written comments were submitted during the 35-day comment period.

MAX/cmw 02/22/12

"Emission Factors Attachment"

Emission Unit	Operating Par	ameter	Pollutant	EF	Units	Ref	Emissions (ton/y
į		'	NOx		lb/hr	ST 4/2010	0.2
Boiler 1 (NE) Tail Gas	7946	hours	co		lb/hr	ST 4/2010	5.7
	7540	hours/			lb/hr	ST 4/2010	9.8
			MeOH		lb/hr	ST 4/2010	1.9
			HCOH		lb/hr	ST 4/2010	0.2
			CO		lb/hr	ST 4/2010	0.0
Boiler 2 (Erie) Tail Gas	5950	hours/			lb/hr	ST 4/2010	1.8
					lb/hr	ST 4/2010	1.2
1		ŀ	MeOH HCOH		lb/hr	ST 4/2010	0.0
					lb/hr	ST 4/2010	0.0
		ł	PM/PM10/PM2.5		Ib/MMSCF		0.7
		i	NOx		lb/MMSCF		10.2
All Boilers Natural Gas	205.4	MMsc	co		lb/MMSCF		8.6
	200.4	IVIIVISC			lb/MMSCF		0.0
			VOC		lb/MMSCF	AP42	0.5
			Total HAP		lb/MMSCF	AP42	0.1
			Non HAP VOC		lb/MMSCF		0.9
		İ	CO		ib/hr	ST 4/2010	0.6
Boiler 1 (NE) Bypass	54	hours/y	r VOC	249.37		ST 4/2010	6.7
			НСОН		lb/hr	ST 4/2010	0.1
			MeOH	49.53		ST 4/2010	1.3
		İ	со		lb/hr	ST 4/2010	1.5
Boiler 2 (Erie) Bypass	50	hours/y	r Voc	43	lb/hr	ST 4/2010	1.0
			нсон	0.61	lb/hr	ST 4/2010	0.02
			MeOH			ST 4/2010	0.0
		1	voc	1.57E-01	lb/ton	R&D	5.89
PF Resin Reacotr Scrubber	75,000	tons/yr	НСОН	2.57E-03		R&D	0.10
,	•		MeOH	2.13E-02	lb/ton	R&D	0.80
			Phenol	2.54E-04		R&D	0.01
ļ .			voc	6.56E-02		R&D	2.46
UF Resin Reactor Scrubber	75,000	tons/yr	нсон	8.97E-04		R&D	0.03
i		101.57 7.	MeOH	7.42E-03		R&D	0.28
-	<u> </u>		Triethylamine	1.10E-02		R&D	0.41
			voc	2.50E-01		R&D	2.19
MF Resin Reactor Scrubber	17,500	tons/yr	НСОН	3.89E-03	$\overline{}$	R&D	0.03
			MeOH	3.41E-02		R&D	
			voc	4.13E-02		AP42 7.1	0.30
Formaldehyde Storage	82,075	tons/yr	нсон	3.55E-02		AP42 7.1	1.70
		1	MeOH	5.82E-03 I		AP42 7.1	1.46
			Voc	5.01E-05 I		AP42 5.2	0.24
Formaldehyde Loading	10,000	tons/yr	нсон	4.29E-05 I		AP42 5.2	0.50
			MeOH	7.15E-06 I			0.43
PF Resin Produced in Reactors	75.000		voc	1.19E-06		AP42 5.2	0.07
11 Nesii 1 Todacea III Neactors	75,000	ton/yr	Ethylene Glycol	1.19E-06 I		site	8.93E-02
MF Resin Produced in Reactors	47.500		VOC			site	8.93E-02
Mir Resili Froduced III Reactors	17,500	tons/yr	Ethylene Glycol	2.89E-03		site	0.03
· · · · · · · · · · · · · · · · · · ·			VOC	1.82E-04		site	1.59E-03
UF Resin Loading	70.000		нсон	3.43E-06 1		AP42 5.2	0.24
OF Resili Loading	70,000	tons/yr	MeOH			AP42 5.2	0.10
		1	Ethylene Glycol	1.98E-06 II		AP42 5.2	0.14
Telopina I andina			VOC	2.16E-09 II		AP42 5.2	1.51E-04
Triazine Loading	5,000	tons/yr	MeOH	2.82E-05 II		AP42 5.2	0.14
			voc	2.71E-05 II		AP42 5.2	0.14
		Į.	нсон	5.13E-05 II		AP42 5.2	3.71
DE D. J. J. J.		Į.	MeOH	1.42E-06 II		AP42 5.2	0.10
PF Resin Loading	72,250	tons/yr	Phenol	2.40E-06 IL		AP42 5.2	0.17
				1.09E-07 II		AP42 5.2	0.01
			Etyhiene Glycol	1.09E-06 lk		AP42 5.2	7.88E-02
			Methyl Isobutyl Ketone VOC	1.52E-07 IL		AP42 5.2	0.01
}		ĺ	нсон	1.14E-04 IL		AP42 5.2	0.26
Durito IV 1050141			MeOH	1.59E-06 IL		AP42 5.2	0.00
Durite LV 1259M Loading	2,250	tons/yr		5.93E-05 Ib		AP42 5.2	0.13
			Phenol Etylogo Chapl	1.22E-07 IL		P42 5.2	2.75E-04
		1	Etyhlene Glycol	2.70E-09 lb		P42 5.2	6.08E-06
	· · · · · · · · · · · · · · · · · · ·		Methyl Isobutyl Ketone	1.70E-07 lb		P42 5.2	3.83E-04
		1	VOC	6.35E-05 lb		P42 5.2	0.03
			нсон	1.47E-06 lb		P42 5.2	7.35E-04
Durite SC748A Loading	500	tons/yr	MeOH	1.29E-05 lb		P42 5.2	0.01
		- [Phenol	1.13E-07 lb		P42 5.2	5.65E-05
1		1	Etyhlene Glycol	2.50E-09 lb		P42 5.2	1.25E-06
			Methyl isobutyl Ketone	1.57E-07 lb		P42 5.2	7.85E-05
1			VOC	1.69E-05 lb		P42 5.2	0.30
MF Resin Loading	17,500	tons/yr	НСОН	9.22E-08 lb		P42 5.2	1.61E-03
ļ			MeOH	1.54E-05 lb		P42 5.2	0.27
Dry Catalyst Loading	2.052		Etyhlene Glycol	3.56E-10 lb		P42 5.2	6.23E-06
	3,893	tons/yr	VOC and HCOH	2.90E-07 lb	/lb A	P42 5.2	1.13E-03
Methanol Loading	250	tons/yr	VOC and MeOH	1.53E-04 lb,		P42 5.2	3.83E-02
HE Parin Staves	7		VOC	6.19E-03 lb,		P42 7.1	0.22
UF Resin Storage	70,000	tons/yr	НСОН	2.34E-03 lb,		P42 7.1	0.08
——— — —			MeOH	3.78E-03 lb,		P42 7.1	0.08
Triazine Storage	5,000	tons/yr	VOC	208.50 lb,		P42 7.1	0.13
		33/13/ 91	MeOH	201.37 lb/		P42 7.1	0.10
			voc	5.66E-03 lb/		P42 7.1	0.10
l l		· · · · ·					
			НСОН				
PF/PRF Resin Storage	75,000			1.81E-04 lb/ 2.90E-03 lb/	ton Ai	P42 7.1 P42 7.1	0.01 0.11

1	1	ı			-r.:		
			Ethylene Glycol Methyl Isobutyl Ketone		5 lb/ton 6 lb/ton	AP42 7.1 AP42 7.1	3.51E-03
		+	VOC		3 lb/ton	AP42 7.1 AP42 7.1	3.08E-04
MF Resin Storage	17,500	tons/yr	***************************************		5 lb/ton	AP42 7.1	1.25E-04
Methanol Storage	42,000	tone/ur	VOC and MeOH	8.18E-0		AP42 7.1	0.07
	72,000	tons/yr	VOC and MeOR	1.26E-0		TANKS 4.09 AP42 7.1	0.26
Methanol Distillate	259	tons/yr		7.42E-0		AP42 7.1	9.61E-04
			MeOH	3.26E-0		AP42 7.1	4.22E-02
Phenol Storage	27,000	tons/yr	VOC	3.85E-02		TANKS 4.09	0.52
Triethylamine Storage	300	tons/yr	VOC		lb/ton	TANKS 4.09	0.52
			Triethylamine		lb/ton	TANKS 4.09	0.18
Triethanolamine Storage Triethanolamine Rx9 Storage	1,487	tons/yr tons/yr		6.55E-03		TANKS 4.09	4.87E-03
10% Formic Acid	4,127	tons/yr		3.26E-03		TANKS 4.09	6.19E-05 2.56E-03
Diethylene Glycol Storage	9,588	tons/yr		3.13E-06		TANKS 4.09	1.50E-05
UF Distillate Storage	2.710	1	voc		lb/yr	AP42 7.1	2.71E-02
Or Distillate Storage	2,718	tons/yr	HCOH MeOH		lb/yr	AP42 7.1	3.43E-03
PF Distillate Storage	5,839	*****	VOC		lb/yr lb/yr	AP42 7.1 AP42 7.1	2.36E-02 1.83E-03
	3,835	tons/yr	нсон		lb/yr	AP42 7.1	1.83E-03
			VOC		lb/yr	AP42 7.1	8.90E-03
PF Washwater Storage	21,605	tons/yr	HCOH MeOH		lb/yr lb/yr	AP42 7.1 AP42 7.1	5.41E-03 3.48E-03
			Phenoi		lb/yr	AP42 7.1	7.43E-06
			voc		lb/yr	AP42 7.1	2.44E-03
UF Seal Water	18,630	tons/yr	HCOH MeOH		lb/yr	AP42 7.1	6.75E-04
	<u></u>		Phenol	3.46E-04	lb/yr lb/yr	AP42 7.1 AP42 7.1	1.76E-03 1.73E-07
GN11 Storage	3,375	tons/yr	VOC and Methanol	2.67E-03		AP42 7.1	4.51E-03
			Voc		lb/yr	AP42 7.1	0.14
Shop-Miller CS 000111		1	HCOH MeOH	27.37	lb/yr	AP42 7.1 AP42 7.1	6.05E-04 0.014
Sheer Mixer RF-300W	23,652,000	gallons/yı	Methyl Isobutyl Ketone		lb/yr	AP42 7.1	3.30E-04
et.			Ethylene Glycol	0.07	lb/yr	AP42 7.1	3.50E-05
			Pheno! VOC		lb/yr	AP42 7.1	1.20E-03
Sheer Mixer FM-6310L	27,422,609	gallons/yr	нсон		lb/yr lb/yr	AP42 7.1 AP42 7.1	5.50E-04 5.50E-04
Sheer Mixer FM-7400L	75,085,714	gallons/yr	voc		lb/yr	AP42 7.1	2.50E-05
	10,-10,11	ganons/y	нсон		lb/yr	AP42 7.1	2.50E-05
Sheer Mixer Momentive 4720	13,770,000	gallons/yr	VOC	288.91	lb/yr lb/yr	AP42 7.1	0.14
		8=,	MeOH		lb/yr	AP42 7.1 AP42 7.1	4.55E-04 0.14
			VOC	440.18		WATER9	0.22
Washwater Pits	1,464,540	gallons/yr	HCOH		lb/yr	WATER9	1.87E-03
			MeOH Phenol		lb/yr lb/yr	WATER9 WATER9	7.20E-04
Stearic Acid Storage	1,431	tons/yr	voc		lb/yr	TANKS 4.09	2.45E-04
Plant #3 Fugitive Emissions	9 999	l. ,	VOC and Total HAPs			Modified SOCMI	1.25
r tant #3 r agitive Ethissions	8,000	hours/yr	MeOH			Modified SOCMI	0.43
···	· · · · · · · · · · · · · · · · · · ·	 	VOC and Total HAPs			Modified SOCMI Modified SOCMI	0.82
Plant #2 Fugitive Emissions	6,000	hours/yr	нснсо			Modified SOCMI	0.26
			MeOH VOC and Tatal Map			Modified SOCMI	0.28
			VOC and Total HAPs HCHCO			Modified SOCMI Modified SOCMI	1.68 0.381
Resin Fugitive Emissions	8,760	hours/yr				Modified SOCMI	0.51
			Phenol			Modified SOCMI	0.66
Urea Weigh Bin #1	25,000	tons/yr	Triethylamine PM/PM10			Modified SOCMI	0.14
Urea Weigh Bin #2	25,000	tons/yr	PM/PM10		lb/ton lb/ton	Vendor Vendor	0.25 0.25
Adhesive Dump Hopper	1,000	tons/yr	PM/PM10		lb/ton	Vendor	1
Melamine Conveyor Melaimine Hopper	455 263		PM/PM10		lb/MMcf	Vendor	0.65
RTU Dry Material Loading	750		PM/PM10 PM/PM10		lb/MMcf_ lb/ton	Vendor EPA 11.17-4	0.38
	411		PM/PM10		lb/MMcf	Vendor	0.23
Dry Catalyst Blender#1	3,893	tons/yr	voc	0.51	lb/yr	Site Estimate	2.55E-04
	561		HCOH	0.27		Site Estimate	1.35E-04
Dry Catalyst Blender#2		1	PM/PM10 VOC	611.47	lb/MMcf lb/vr	Vendor Site Estimate	0.80 0.31
	1,560	hours/yr	нсон	611.24		R&D Study	0.31
Dry Catalyst Vacuum Sweeper	15.4		PM/PM10	2.86	lb/MMcf	Vendor	0.02
Dry Catalyst Exhaust Fan West Dry Catalyst Exhaust Fan South	18.7		PM/PM10 PM/PM10		lb/MMcf	Site Estimate	0.01
Unpaved Haul Road	54	VMT	PM/PM10		lb/MMcf lb/VMT	Site Estimate Ap42	0.01 0.19
			voc	0.00861		Company Study	2.58
Resin Drying Pad	300	tons/yr	нсон	0.00606		Company Study	1.82
			MeOH Phenoi	0.00252		Company Study	0.76
Emulsified Wax Process		tana/	MeOH	0.00003		Company Study Site Estimate	0.01 5.00E-06
Emalonica Wax Floress	71,540	tons/yr	voc	0.05	lb/yr	Site Estimate	2.50E-05
Emulsified Wax Loading	74.540	tons/yr	MeOH	9.07	lb/yr	Site Estimate	0.005
Emploite - days	71,540	+	VOC MeOH	137.0		Site Estimate	0.069
Emulsified Wax Storage	71,540	tons/yr	VOC	2.03		Site Estimate Site Estimate	1.02E-03 1.02E-03
Wax Process (includes emulsified	71,540	tons/yr	Toluene	1302.00	lb/yr	Site Estimate	0.65
wax and process slack wax storage		, y,					
	<u></u>		voc	1302.0	b/yr	Site Estimate	0.65

Emission Unit	PM/PM10	DM2 5	NOx	lco	llutant VOC	нсно	MacOll	Dhar -!
Boiler 1 (Erie) Tail Gas	PIVI/PIVIIO	PIVIZ.3					MeOH	Phenol
Boiler 2 (NE) Tail Gas			0.20	5.7				
All Boilers Natural Gas	0.78	0.78	0.09 10.27	1.8 8.6			0.02	
Boiler 1 (Erie) Bypass	0.78	0.78	10.27				4.04	
Boiler 2 (NE) Bypass				0.6		 		
PF Resin Reacotr Scrubber	 			1.5		 	0.01	0.00
UF Resin Reactor Scrubber					5.89			0.01
MF Resin Reactor Scrubber	 -				2.46		0.28	
Formaldehyde Storage					2.19		0.30	
Formaldehyde Loading	+				1.70		0.24	
PF Resin Produced in Reactors	+				0.50		0.07	0.01
MF Resin Produced in Reactors					0.03			0.01
UF Resin Loading	 				0.03		0.14	
PF Resin Loading	-				3.71			
Durite LV 1259M Loading	 			-	0.26	0.10	0.17	
Durite SC748A Loading							0.13	2.75E-04
MF Resin Loading					0.03			5.65E-05
Dry Catalyst Loading	+				0.30		0.27	
Methanol Loading	 				1.13E-03		0.04	
UF Resin Storage					3.83E-02		0.04	-
PF/PRF Resin Storage	+				0.22		0.13	1 505 00
MF Resin Storage						0.01 1.25E-04	0.11	1.56E-03
Methanol Storage	-				0.07	1.25E-04	0.07	
Methanol Distillate					0.26		0.26	
Phenol Storage					0.04		4.22E-02	0.50
Triethylamine Storage					0.52			0.52
Triethanolamine Rx9 Storage	-		-		1.77E-01 6.19E-05			····
10% Formic Acid					+			
Diethylene Glycol Storage	 				2.56E-03 1.50E-05			
UF Distillate Storage	 	-			2.71E-02	3.43E-03	2 265 02	
PF Distillate Storage	 			,	1.83E-03		2.36E-02	
PF Washwater Storage	 				8.90E-03		3.48E-03	7.425.06
UF Seal Water					2.44E-03		1.76E-03	7.43E-06 1.73E-07
GN11 Storage	1	-			4.51E-03		4.51E-03	1./3E-0/
Sheer Mixer RF-300W	+				0.14		0.014	1.20E-03
Sheer Mixer FM-6310L	-				5.50E-04		0.014	1.20E-03
Sheer Mixer FM-7400L	-				2.50E-05	2.50E-05		
Sheer Mixer Momentive 4720	+				0.14	4.55E-04	0.14	
Washwater Pits	 				0.14	1.87E-03	0.14	7.20E-04
Stearic Acid Storage		-	-		1.25	1.071-03	0.22	7.20E-04
Plant 3 Fugitives	_				1.25	0.43	0.82	
Plant 2 Fugitives	 			· · ·	0.54	0.45	0.82	
Resin Fugitives	 				1.68	0.381	0.28	0.14
Urea Weigh Bin #1	0.25	-	-		1.08	0.361	0.51	0.14
Jrea Weigh Bin #2	0.25				+			
Adhesive Dump Hopper	1					***		
Melamine Conveyor	0.65				+			
Melaimine Hopper	0.38				+			
RTU Dry Material Loading	0.23				 			
Ory Catalyst Blender#1	0.59					1.35E-04		
Ory Catalyst Blender#2	0.80				 	0.31		
Ory Catalyst Vacuum Sweeper	0.02				+	0.51		
Ory Catalyst Exhaust Fan West	0.02				-			
Ory Catalyst Exhaust Fan South	0.01							
Jnpaved Haul Road	0.01							
Resin Drying Pad	0.19				 	1 00		
Emulsified Wax Process				.		1.82	0.76	
Emulsified Wax Loading	 				 		5.00E-06	
Wax Process	+				0.65		0.004535	

9.20